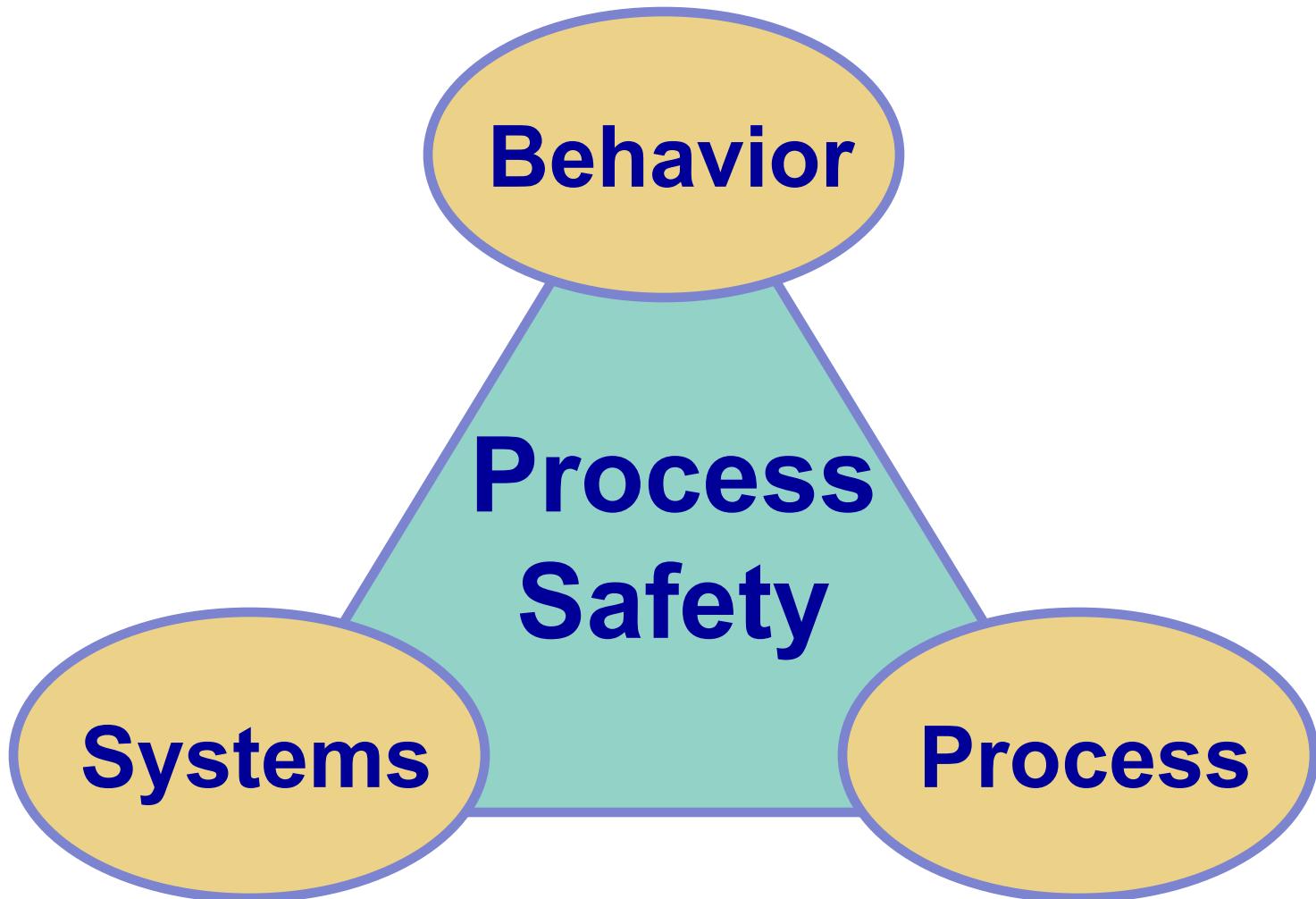


# **Overview of Process Safety, Green Engineering, and Inherently Safer Design**

Harry J. Toops LSU Department of Chemical Engineering with significant material from SACHE 2003 Workshop presentation entitled: *Inherently Safer Design*, by Dennis Hendershot Rohm and Haas Company

# Three Elements of Process Safety



# Process Safety Milestone Practices

Pre-1930's

Identify who caused the loss  
and punish the guilty

**Behavior**

Pre-1970's

Find breakdown in, and fix  
man-machine interface

**Process**

1970's, 80's

Development of risk  
assessment techniques and  
systematic approaches

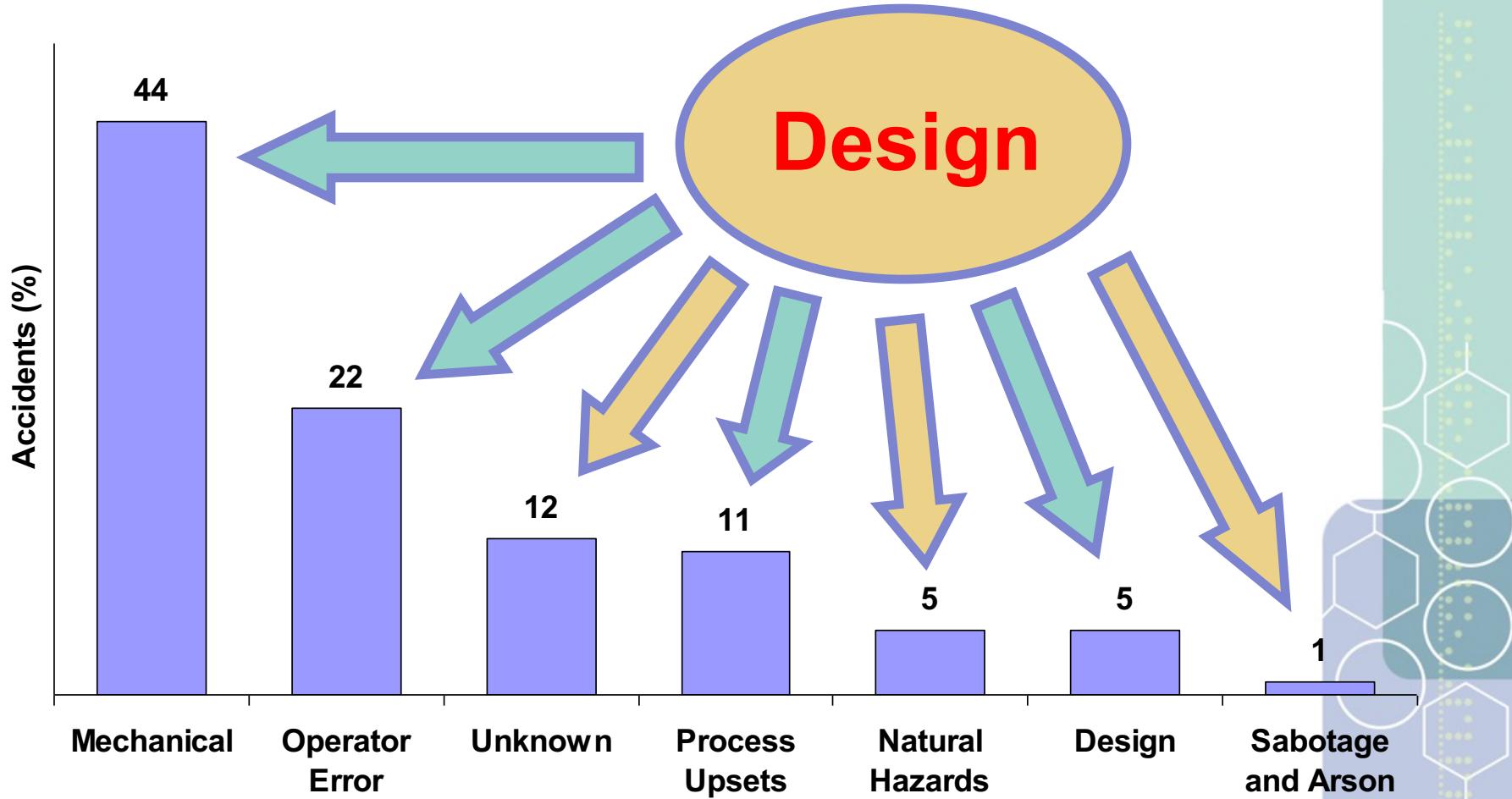
**Mgmt Systems**

1980's +

Performance-, risk-based  
standards, regulations;  
**Comprehensive**  
'green' and 'inherent' designs



# Causes of Losses in Large Plant Accidents



# Green chemistry and engineering – A Definition

*The design, commercialization, and use of chemical processes and products, which are feasible and economical while minimizing:*

- 1) generation of pollution at the source, and*
- 2) risk to human health and the environment.*

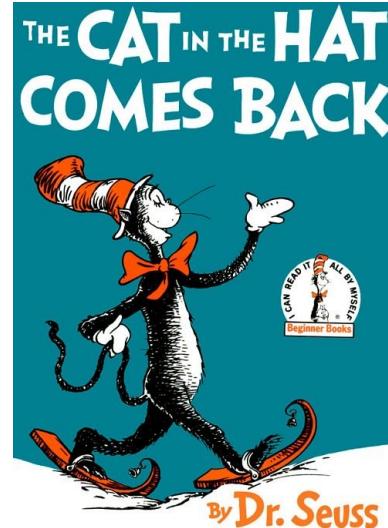
# New paradigm for the environment

- Traditional environmental approach
  - “End of pipe” waste treatment
  - “Waste minimization” – an advance, but we can go further
- Green chemistry and engineering
  - Eliminate or dramatically reduce hazards to the environment

# Many of us learned this as children

- Dr. Suess –

*The Cat in the Hat  
Comes Back*



- “Once you get *something* dirty, the only way to get it clean is to make *something else* dirty.”
- The best way to keep the world clean is to not get it dirty to begin with.

# Inherently Safer Design – A Definition

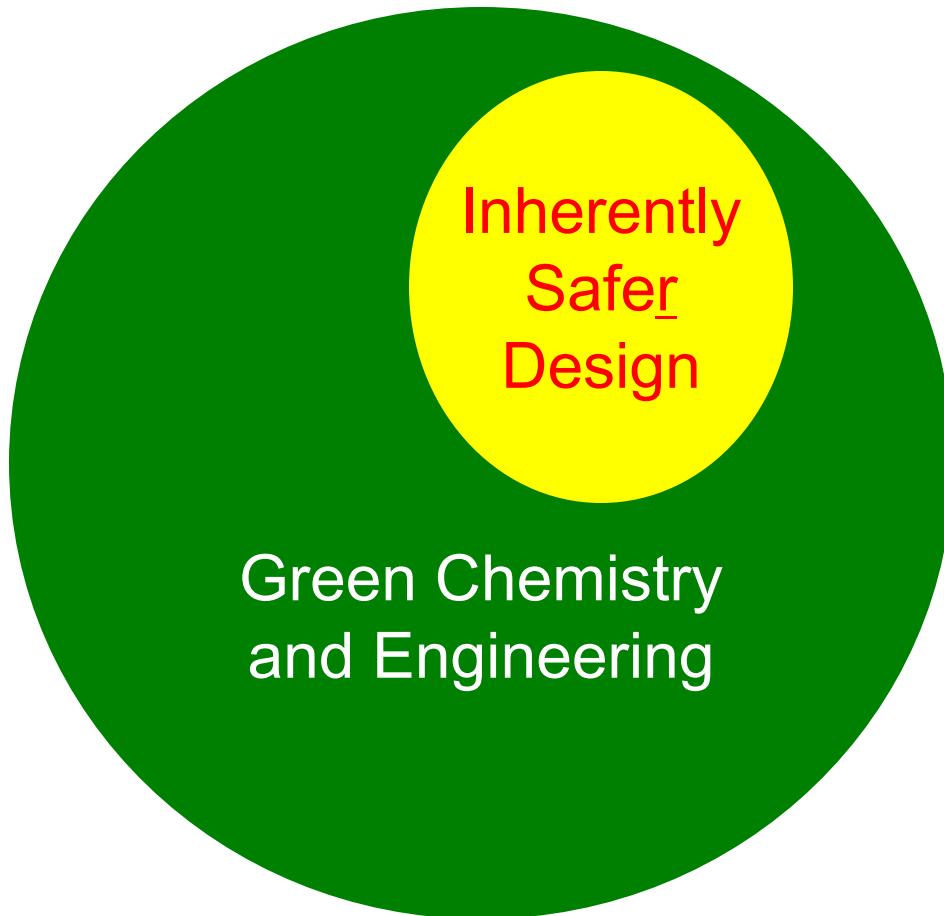
*The design of chemical processes and products with specific attention to eliminating hazards from the manufacturing process rather than relying on the control of these hazards*

**Notice the common philosophy to Green Engineering?**

# New paradigm for safety

- Traditional safety approach
  - “Add on” safety features
    - *Prevent* - alarms, safety interlocks, procedures, training
    - *Mitigate* – sprinkler systems, water curtains, emergency response systems and procedures
- Inherently safer design
  - *Eliminate or significantly reduce process hazards*

# Inherently safer design, green chemistry, and green engineering

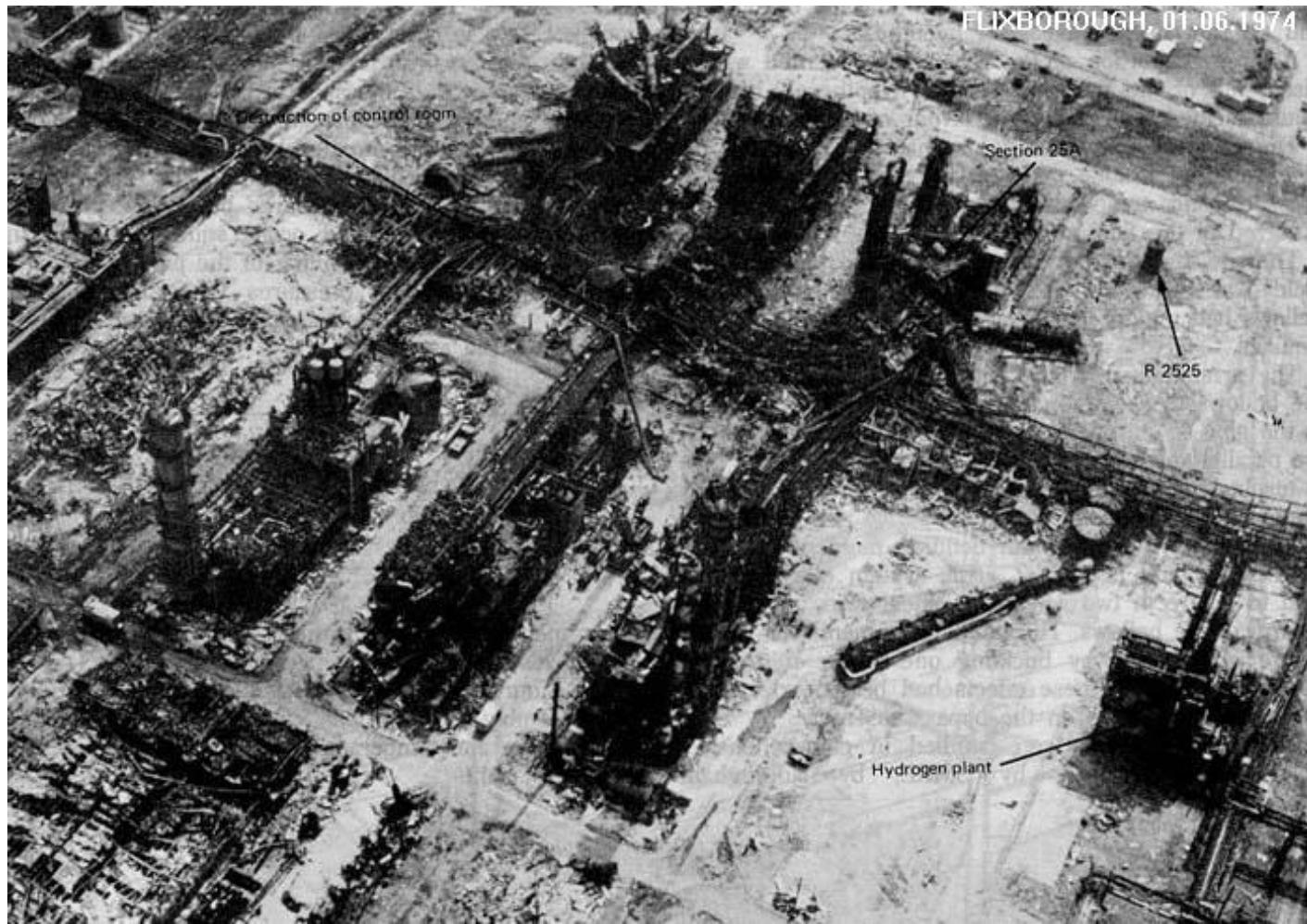


# Why are we interested in inherently safer design?

# Flixborough, England (1974)



# Flixborough, England (1974)



# Henderson, Nevada, (1988)



# What is inherently safer design?

- ***Inherent*** - “existing in something as a permanent and inseparable element...”
  - safety “built in”, not “added on”
- **Eliminate or minimize hazards rather than control hazards**
- **More a philosophy and way of thinking than a specific set of tools and methods**
  - Applicable at all levels of design and operation from conceptual design to plant operations
- **“*Safer*,” not “*Safe*”**

# Hazard

- **An inherent physical or chemical characteristic that has the potential for causing harm to people, the environment, or property (CCPS, 1992).**
- **Hazards are intrinsic to a material, or its conditions of use.**
- **Examples**
  - **Phosgene - toxic by inhalation**
  - **Acetone - flammable**
  - **High pressure steam - potential energy due to pressure, high temperature**

# To eliminate hazards:

- Eliminate the material
- Change the material
- Change the conditions of use



# Chemical Process Safety Strategies

# Inherent

- **Eliminate or reduce the hazard by changing to a process or materials which are non-hazardous or less hazardous**
- **Integral to the product, process, or plant - cannot be easily defeated or changed without fundamentally altering the process or plant design**
- **EXAMPLE**
  - **Substituting water for a flammable solvent (latex paints compared to oil base paints)**

# Passive

- **Minimize hazard using process or equipment design features which reduce frequency or consequence without the active functioning of any device**
- **EXAMPLE**
  - **Containment dike around a hazardous material storage tank**

# Active

- **Controls, safety interlocks, automatic shut down systems**
- **Multiple active elements**
  - Sensor - detect hazardous condition
  - Logic device - decide what to do
  - Control element - implement action
- **Prevent incidents, or mitigate the consequences of incidents**
- **EXAMPLE**
  - High level alarm in a tank shuts automatic feed valve
- **Caution: Even protective systems can cause incidents! (See *Hendershot et al* handouts)**

# Procedural

- **Standard operating procedures, safety rules and standard procedures, emergency response procedures, training**
- **EXAMPLE**
  - Confined space entry procedures

# Batch Chemical Reactor Example

## Hazard of concern

- *Runaway reaction causing high temperature and pressure and potential reactor rupture*

# Passive

- Maximum adiabatic pressure for reaction determined to be 150 psig
- Run reaction in a 250 psig design reactor
- Hazard (pressure) still exists, but passively contained by the pressure vessel

# Active

- Maximum adiabatic pressure for 100% reaction is 150 psig, reactor design pressure is 50 psig
- Gradually add limiting reactant with temperature control to limit potential energy from reaction
- Use high temperature and pressure interlocks to stop feed and apply emergency cooling
- Provide emergency relief system

# Procedural

- Maximum adiabatic pressure for 100% reaction is 150 psig, reactor design pressure is 50 psig
- Gradually add limiting reactant with temperature control to limit potential energy from reaction
- Train operator to observe temperature, stop feeds and apply cooling if temperature exceeds critical operating limit

# Inherent

- Develop chemistry which is not exothermic, or mildly exothermic
  - Maximum adiabatic exotherm temperature < boiling point of all ingredients and onset temperature of any decomposition or other reactions

# Which strategy should we use?

- **Generally, in order of robustness and reliability:**
  - Inherent
  - Passive
  - Active
  - Procedural
- **But - there is a place and need for ALL of these strategies in a complete safety program**

# Inherently Safer Design Strategies

# Inherently Safer Design Strategies

- **Minimize**
- **Moderate**
- **Substitute**
- **Simplify**

# Minimize

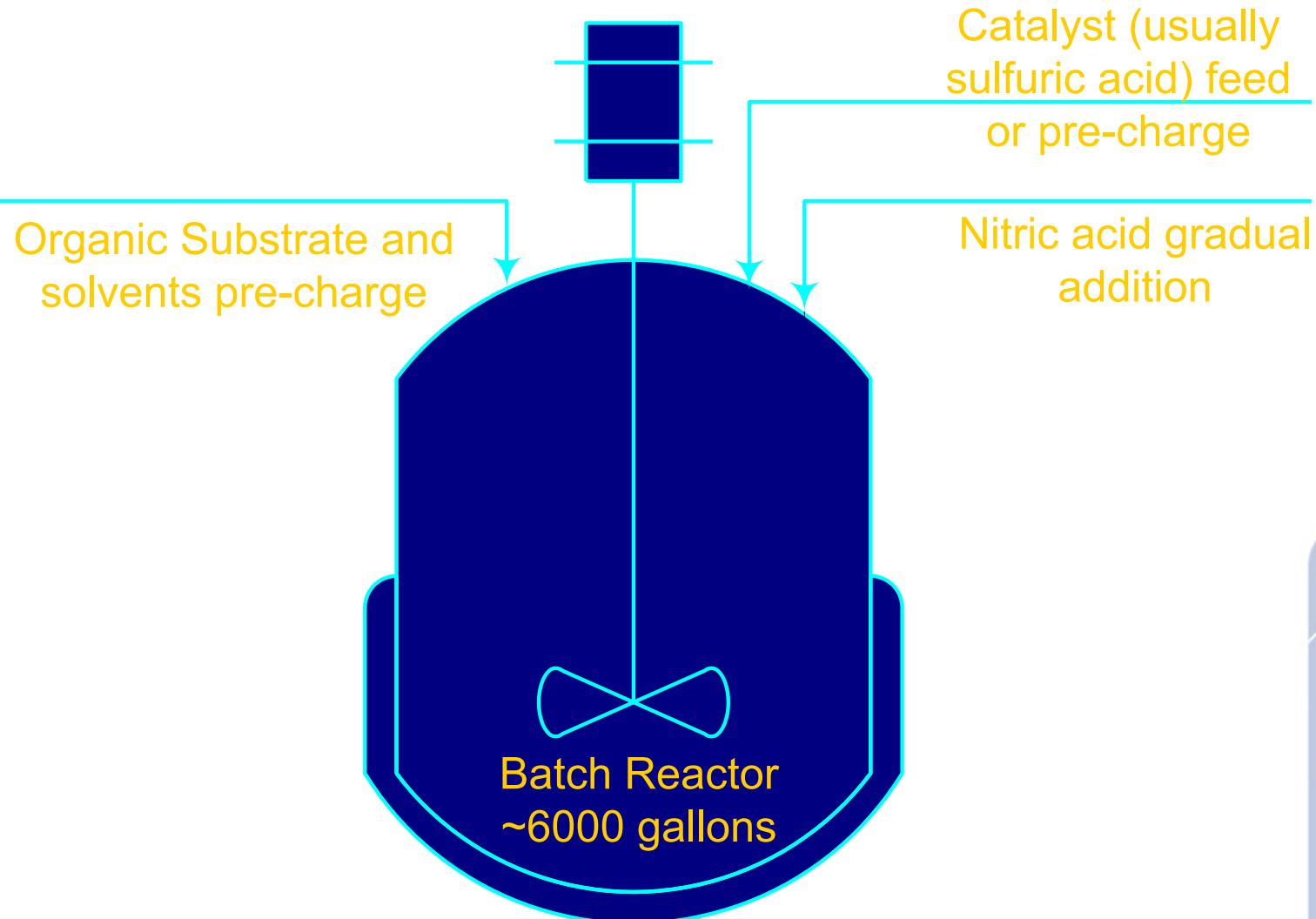
- Use small quantities of hazardous substances or energy
  - Storage
  - Intermediate storage
  - Piping
  - Process equipment
- “Process Intensification”



# Benefits

- **Reduced consequence of incident (explosion, fire, toxic material release)**
- **Improved effectiveness and feasibility of other protective systems – for example:**
  - **Secondary containment**
  - **Reactor dump or quench systems**

# Semi-batch nitration process



# How can Process Intensification be used in this reaction?

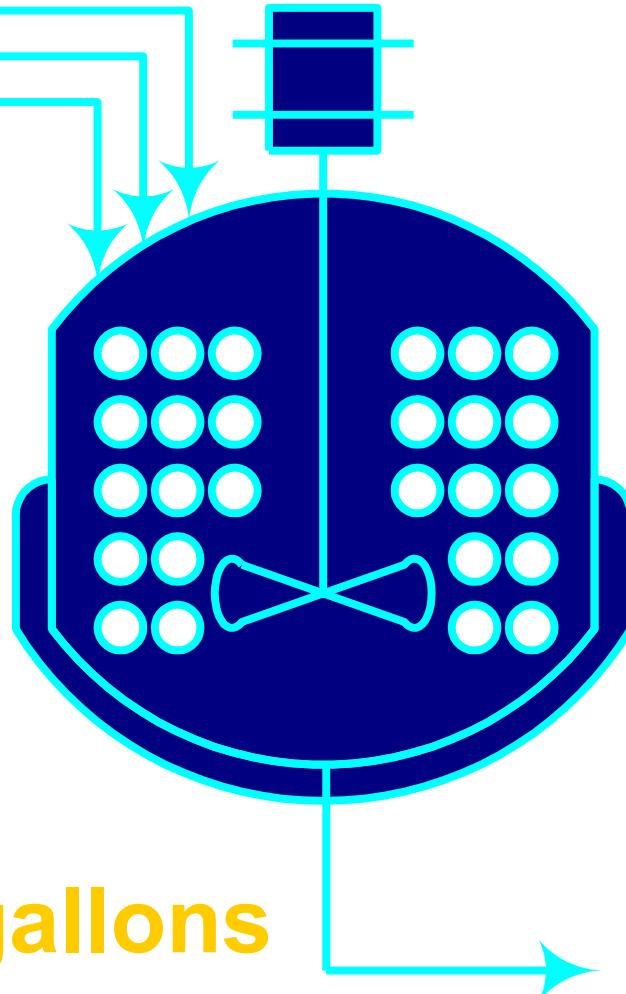
- Mixing – bringing reactants into contact with each other
- Mass transfer – from aqueous phase (nitric acid) to organic phase (organic substrate)
- Heat removal

# CSTR Nitration Process

Raw  
Material  
Feeds

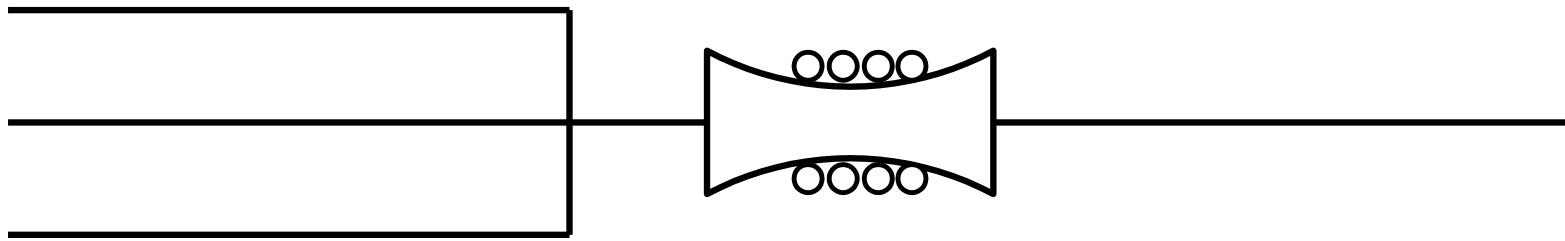
Organic substrate  
Catalyst  
Nitric Acid

Reactor ~ 100 gallons



Product

# One step further: Do this reaction in a pipe reactor?

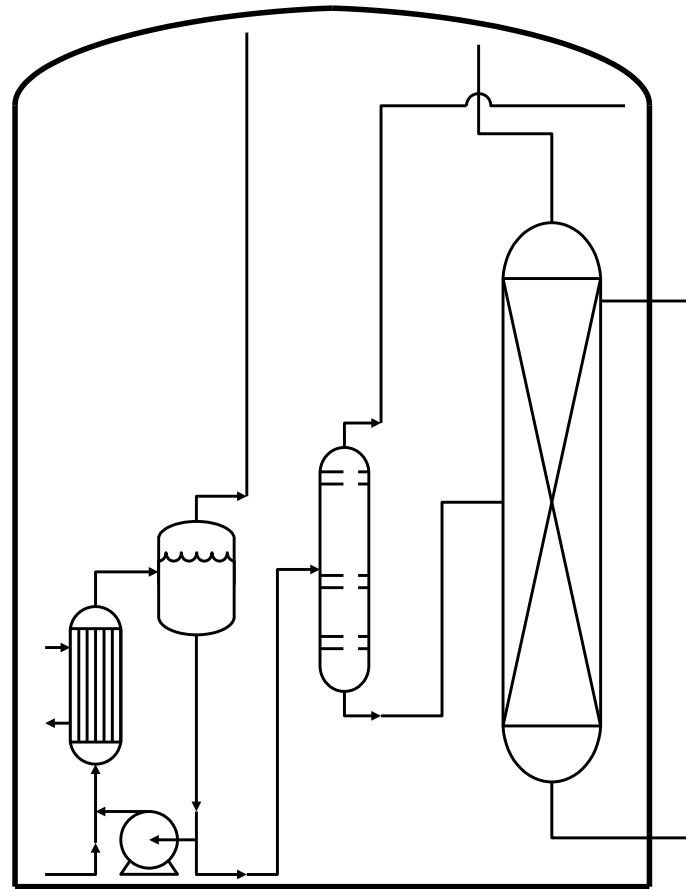


**Raw  
Material  
Feeds**

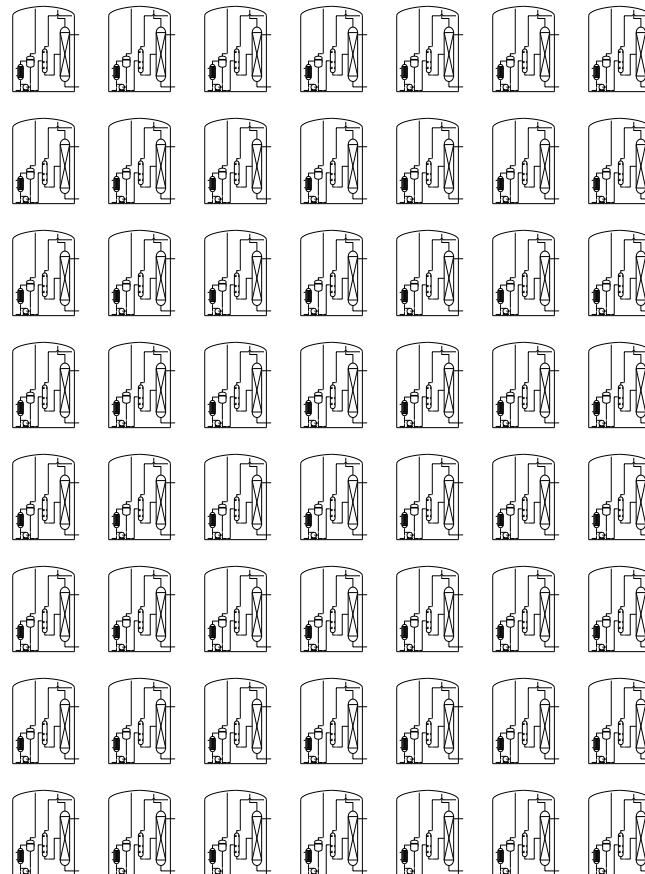
**Organic substrate  
Catalyst  
Nitric Acid**

**Cooled continuous  
mixer/reactor**

# Scale up



# Scale out



# On-demand phosgene generation

- Continuous process to produce phosgene
- Phosgene consumers are batch processes
- No phosgene storage
- Engineering challenges
  - Rapid startup and shutdown
  - Quality control
  - Instrumentation and dynamic process control
  - Disposal of “tail gas” and inerts

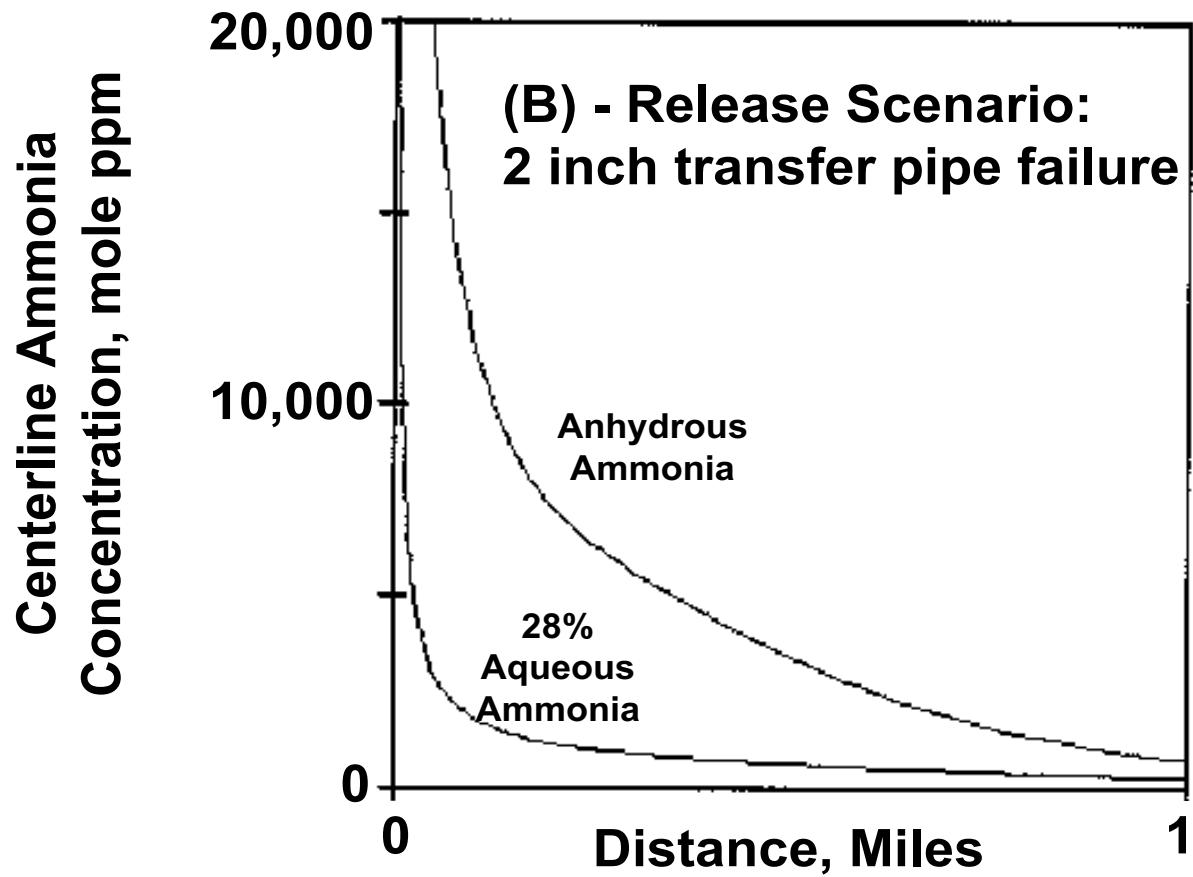
# Moderate

- Dilution
- Refrigeration
- Less severe processing conditions
- Physical characteristics
- Containment
  - Better described as “passive” rather than “inherent”

# Dilution

- Aqueous ammonia instead of anhydrous
- Aqueous HCl in place of anhydrous HCl
- Sulfuric acid in place of oleum
- Wet benzoyl peroxide in place of dry
- Dynamite instead of nitroglycerine

# Effect of dilution



# Less severe processing conditions

- **Ammonia manufacture**
  - 1930s - pressures up to 600 bar
  - 1950s - typically 300-350 bar
  - 1980s - plants operating at pressures of 100-150 bar were being built
- **Result of understanding and improving the process**
- **Lower pressure plants are cheaper, more efficient, as well as safer**

# Substitute

- Substitute a less hazardous reaction chemistry
- Replace a hazardous material with a less hazardous alternative

# Substitute materials

- **Water based coatings and paints in place of solvent based alternatives**
  - Reduce fire hazard
  - Less toxic
  - Less odor
  - More environmentally friendly
  - Reduce hazards for end user and also for the manufacturer

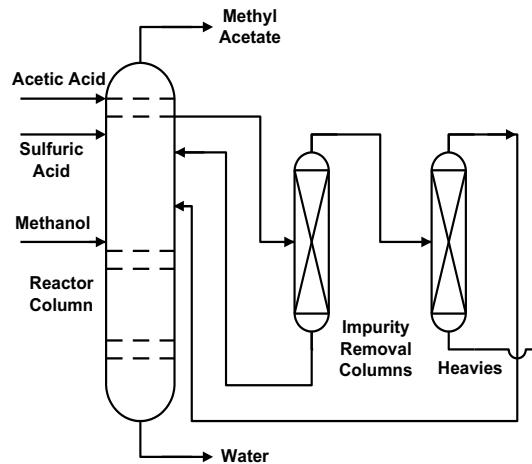
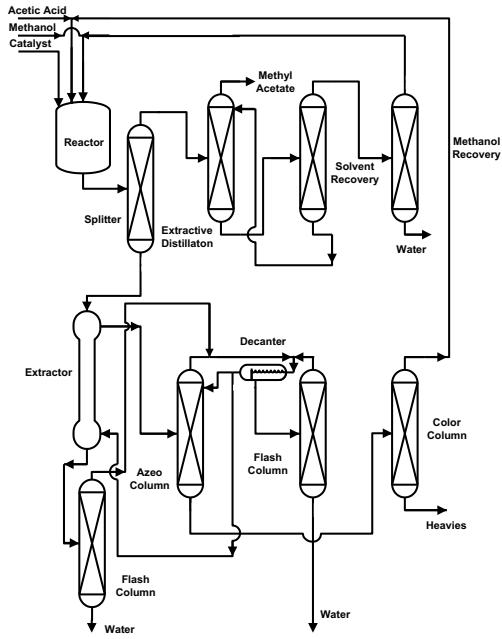
# Simplify

- Eliminate unnecessary complexity to reduce risk of human error
  - **QUESTION ALL COMPLEXITY! Is it really necessary?**



# Simplify - eliminate equipment

- **Reactive distillation methyl acetate process (Eastman Chemical)**
- **Which is simpler?**



# Modified methyl acetate process

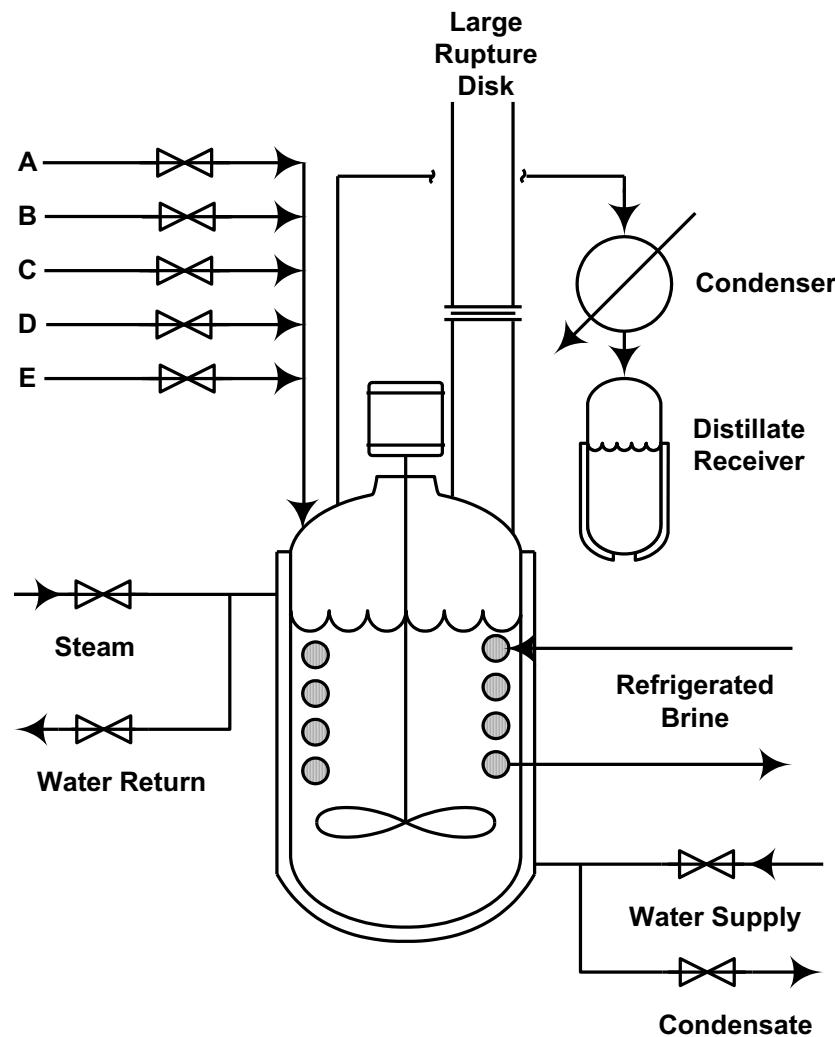
- **Fewer vessels**
- **Fewer pumps**
- **Fewer flanges**
- **Fewer instruments**
- **Fewer valves**
- **Less piping**
- .....

# But, it isn't simpler in every way

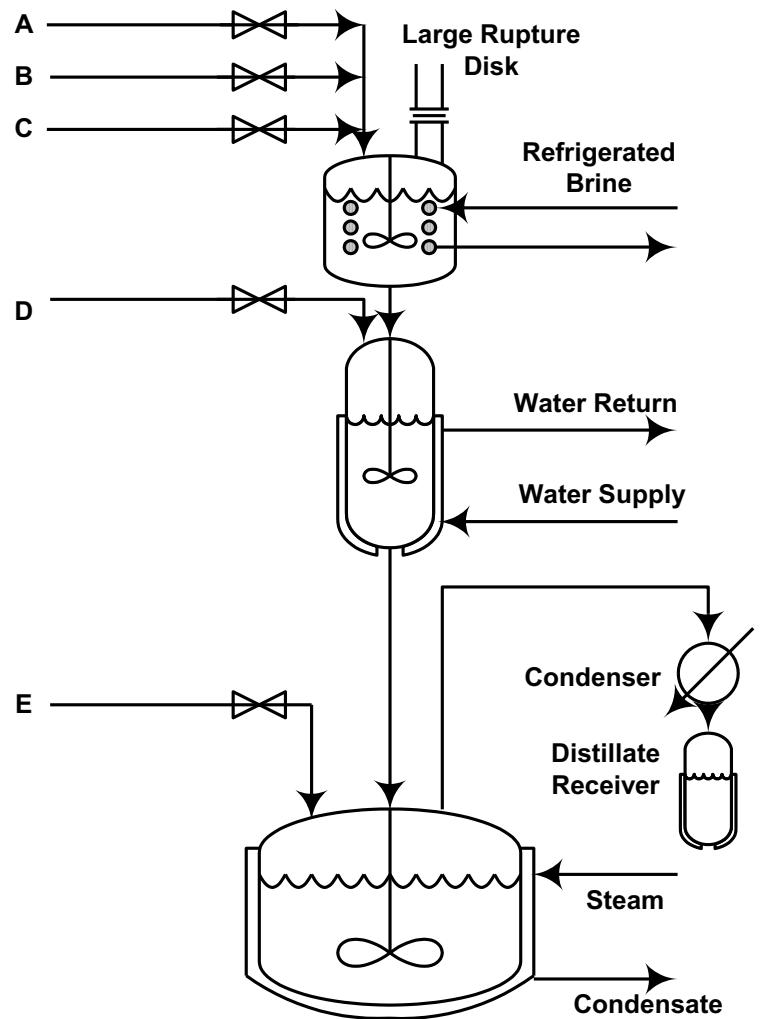
- Reactive distillation column itself is more complex
- Multiple unit operations occur within one vessel
- More complex to design
- More difficult to control and operate



# Single, complex batch reactor



# A sequence of simpler batch reactors for the same process



# Inherent safety conflicts

- In the previous example
  - Each vessel is simpler
- But
  - There are now three vessels, the overall plant is more complex in some ways
  - Compare to methyl acetate example
- Need to understand specific hazards for each situation to decide what is best

# Conflicts and Tradeoffs

# Some problems

- The properties of a technology which make it hazardous may be the same as the properties which make it useful:
  - Airplanes travel at 600 mph
  - Gasoline is flammable
    - Any replacement must have the ability to store a large quantity of energy in a compact form
  - Chlorine is toxic
- Control of the hazard is the critical issue in safely getting the benefits of the technology

# Multiple hazards

- **Everything has multiple hazards**
  - **Automobile travel**
    - **velocity (energy), flammable fuel, exhaust gas toxicity, hot surfaces, pressurized cooling system, electricity.....**
  - **Chemical process or product**
    - **acute toxicity, flammability, corrosiveness, chronic toxicity, various environmental impacts, reactivity.....**

# What does inherently safer mean?

- **Inherently safer is in the context of one or more of the multiple hazards**
- **There may be conflicts**
  - Example - CFC refrigerants
    - low acute toxicity, not flammable
    - potential for environmental damage, long term health impacts
    - Are they inherently safer than alternatives such as propane (flammable) or ammonia (flammable and toxic)?

# **Inherently safer hydrocarbon based refrigerators?**

- Can we redesign the refrigeration machine to minimize the quantity of refrigerant sufficiently that we could still regard it as inherently safer?
  - Home refrigerators – perhaps (<120 grams)
  - Industrial scale applications – probably not, need to rely on passive, active, procedural risk management strategies

# Multiple impacts

- Different populations may perceive the inherent safety of different technology options differently
- Example - chlorine handling - 1 ton cylinders vs. a 90 ton rail car
  - A neighbor two miles away?
  - An operator who has to connect and disconnect cylinders 90 times instead of a rail car once?
- Who is right?

# Inherently safer ≠ safer

- Air travel
  - several hundred people
  - 5 miles up
  - control in 3 dimensions
  - 600 mph
  - thousands of gallons of fuel
  - passengers in a pressure vessel
  - .....
- Automobile travel
  - a few people
  - on the ground
  - control in 2 dimensions
  - 60 mph
  - a few gallons of fuel
  - might even be a convertible
  - .....

- **Automobile travel is inherently safer**
- **But, what is the safest way to travel from Washington to Los Angeles?**
- **Why?**

# At what level of design should engineers consider inherently safer design?

- Selecting Technology? Plant Design? Equipment Details? Operations?
- Best answer? – All levels!
- Inherently safer design *is not* a meeting.
- Inherently safer design *is a way of thinking*, a way of approaching technology design at every level of detail – part of the daily thought process.

# Questions a designer should ask when he has identified a hazard

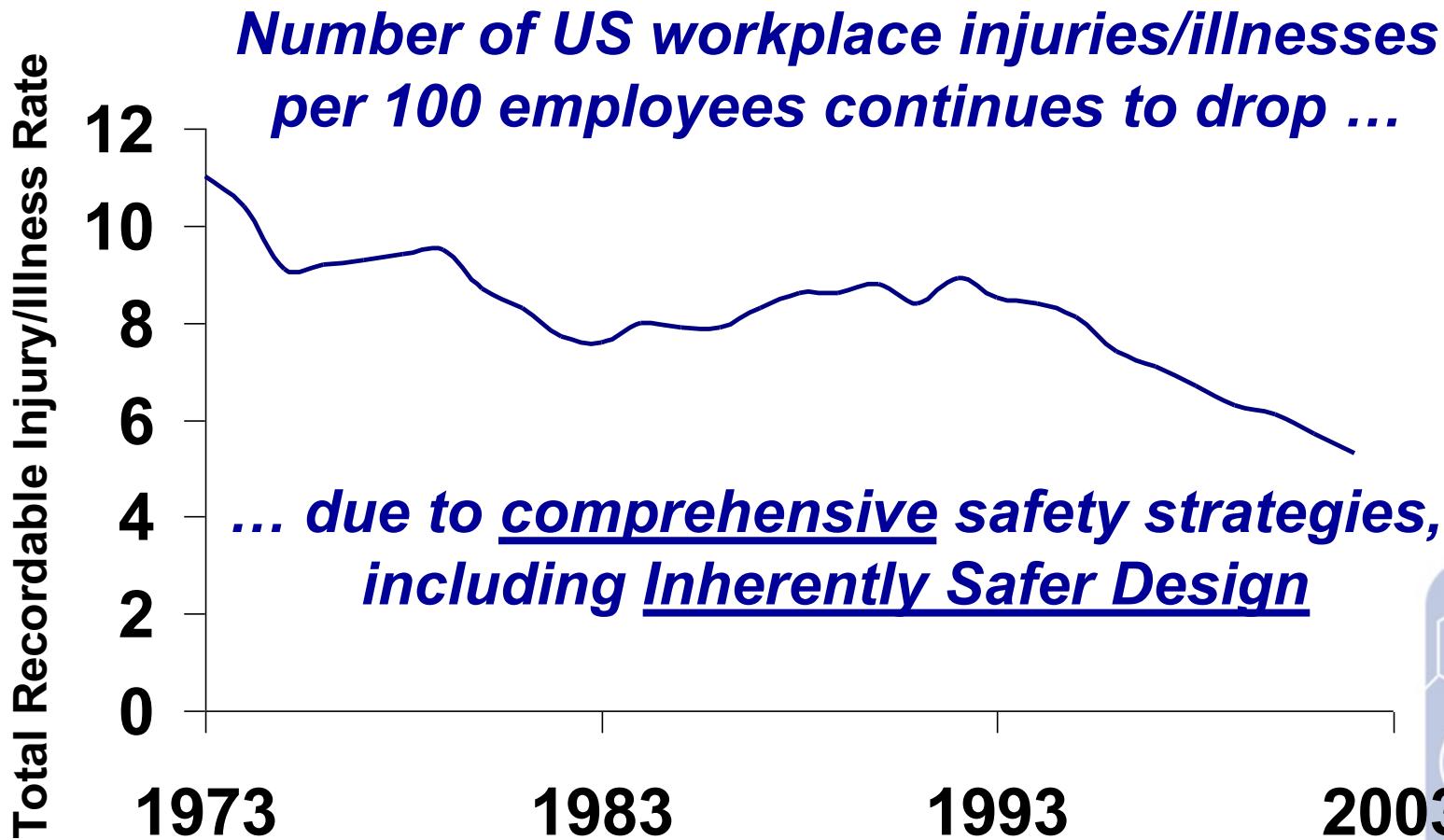
**In this order**

1. Can I eliminate this hazard?
2. If not, can I reduce the magnitude of the hazard?
3. Do the alternatives identified in questions 1 and 2 increase the magnitude of any other hazards, or create new hazards?
4. At this point, what technical and management systems are required to manage the hazards which inevitably will remain?

# The Future: Inherently safer design

- Some hazardous materials and processes can be eliminated or the hazards dramatically reduced.
- The useful characteristics of other materials or processes make their continued use essential to society for the foreseeable future ... we will continue to manage the risks.
- E.g., Air travel

# Is It Worth the Effort?



# **END OF PRESENTATION**